

## Increased TAME From Refinery and Steam Cracker C<sub>5</sub> Feeds



### Technology Profile

**Overview** The *CDIsotame* process combines skeletal isomerization and etherification steps to maximize the production of TAME from refinery and steam cracker C<sub>5</sub> streams. The *CDIsotame* process is one of a family of process technologies developed and commercialized by Catalytic Distillation Technologies (CDTECH) for license to the petroleum refining and petrochemical industries. CDTECH is a partnership between Lummus Technology, a CB&I company, and Chemical Research & Licensing, a CRI company.

**TAME Synthesis-General** TAME is formed by the catalytic etherification of reactive isoamylenes with methanol. Skeletal isomerization increases TAME production from an olefinic C<sub>5</sub> stream by converting normal amylenes to isoamylenes.

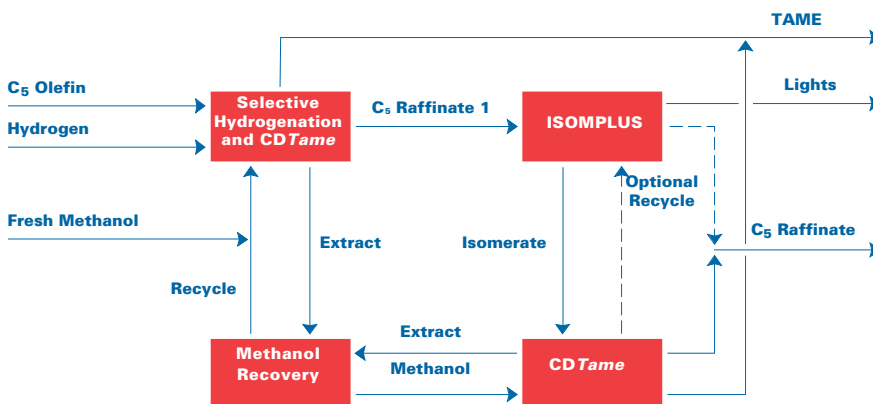
The optimum process configuration is presented below. This scheme provides the minimum capital cost at about 80% C<sub>5</sub> olefin reduction. The olefinic C<sub>5</sub> stream is fed to a selective hydrogenation step where dienes are converted to olefins. Removal of dienes reduces color and gum formation in the TAME product. In addition, unreactive 3MB1 is converted to reactive isoamylenes via hydroisomerization, thus increasing the TAME yield. The primary TAME product is made in the first *CDTame* unit where greater than 90% conversion of isoamylenes is achieved.

Raffinate 1 from the first *CDTame* unit is fed to a skeletal isomerization unit (ISOMPLUS®) where normal pentenes are converted to isoamylenes at high yield and selectivity. The vapor phase reaction takes place over a robust catalyst with long cycles between regenerations.

The isomerate is then fed to a second *CDTame* unit where additional TAME is produced at greater than 95% conversion of isoamylenes. Even higher conversion of normal pentenes to TAME can be achieved by an optional raffinate 2 recycle to the skeletal isomerization unit. A purge stream serves to remove the saturated C<sub>5</sub>s from the recycle stream.

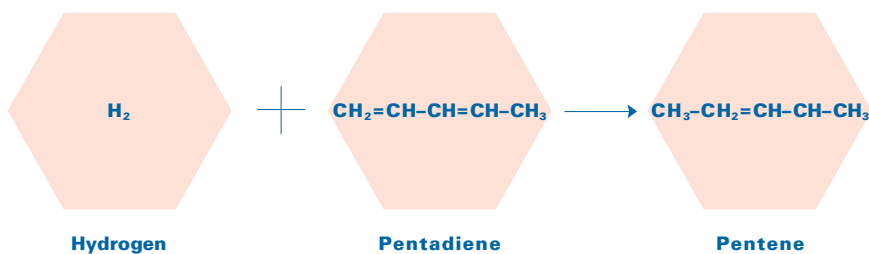
A common methanol recovery unit serves both *CDTame* units.

### CDIsotame Block Flow Diagram

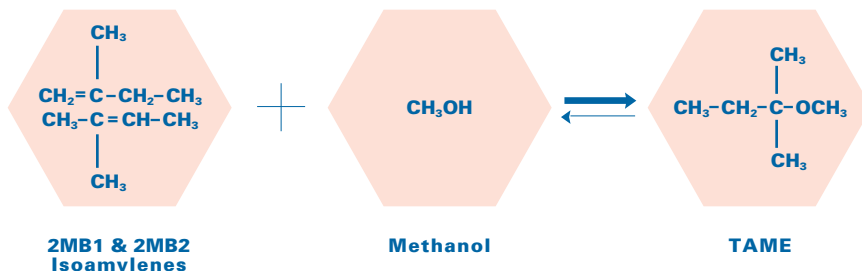


## Process Chemistry

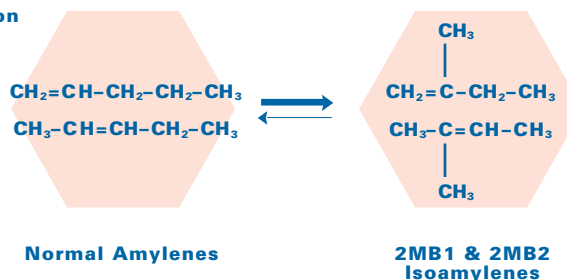
## Selective Hydrogenation



## Etherification



## Skeletal Isomerization



## Advantages

## CDIsotame offers:

Selective hydrogenation of diolefins at minimum capital cost

High conversion of isoamylenes (>95%)

High conversion of normal pentenes (>70 %)

High selectivity of isomerization (>90 %)

Isomerization of 3MB1 to reactive isoamylyene

Improved C<sub>5</sub> raffinate as gasoline feedstock due to reduced

- Color
- Gum formation
- Olefin content

Increased TAME production

Increased gasoline pool octane

Decreased gasoline pool RVP

Low capital and operating cost

Superior economics and performance over C<sub>5</sub> alkylation

High quality TAME product without objectionable odor or color

## Typical Overall Material Balance

Feeds	LB/HR
C <sub>5</sub> S (Pentenes 50 wt. %)	102,133
Methanol	17,700
Hydrogen	29
Products	
C <sub>5</sub> Raffinate	55,006
TAME product	63,410
Light ends (C <sub>4</sub> -)	1,446

TAME Product Composition (excluding C<sub>6</sub>+)

	Wt. %
C <sub>5</sub> S	<1.0
Methanol	<0.1
Di-isoamylyene	0.5
TAA	0.4
TAME	95.6
MTBE	2.4
<b>Total</b>	<b>100.0</b>

CDTECH

3010 Briarpark Drive

Houston, TX 77042 USA

Tel: 713-821-5181

Fax: 713-821-3587